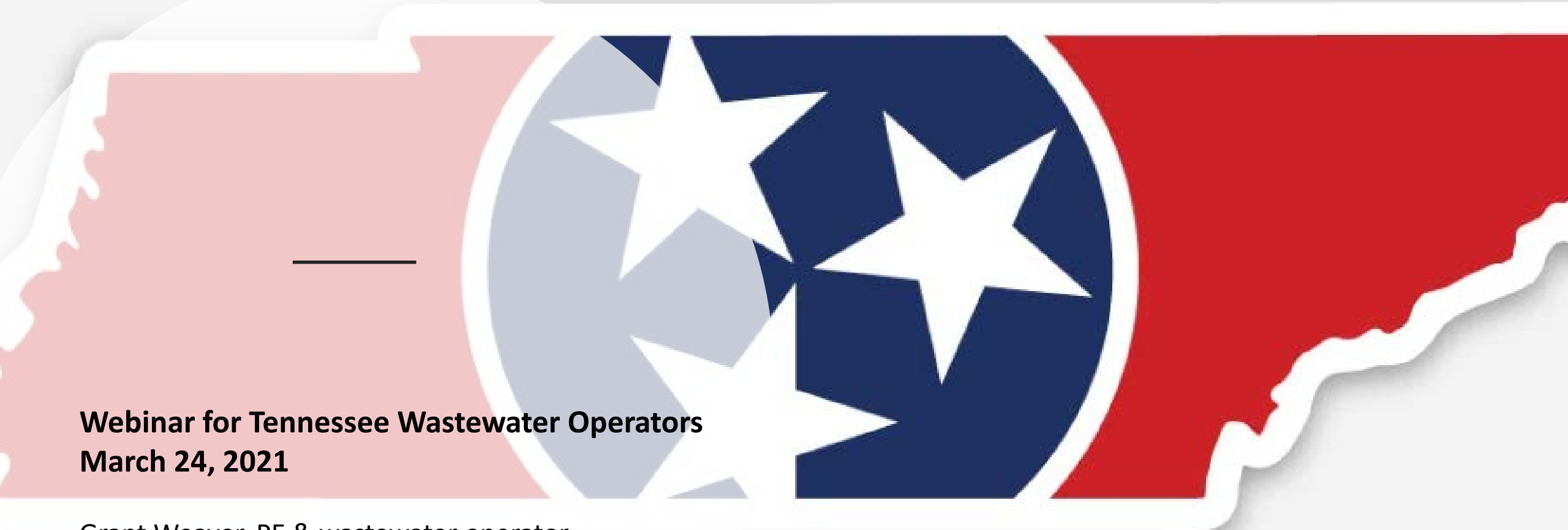


# Brainstorming Nutrient Optimization Opportunities with Tennessee Volunteers

A stylized graphic of the state of Tennessee. The left portion is light red, the right portion is dark red, and the center features a circular emblem with a blue background and white stars, mimicking the state flag. A white outline follows the state's border.

**Webinar for Tennessee Wastewater Operators**  
**March 24, 2021**

Grant Weaver, PE & wastewater operator  
President

CleanWaterOps

G.Weaver@CleanWaterOps.com



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## Strategies for Optimizing Nutrient Removal

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Week 1: Nitrogen Removal

Week 2: Phosphorus Removal

Week 3: N&P Review and Case Studies

Week 4: N&P Removal in Oxidation Ditches

Week 5: N&P Removal in SBRs

Week 6: N&P Removal in Activated Sludge wwtps

**Today: Brainstorming Nutrient Removal Opportunities for Tennessee Wastewater Treatment Plants**



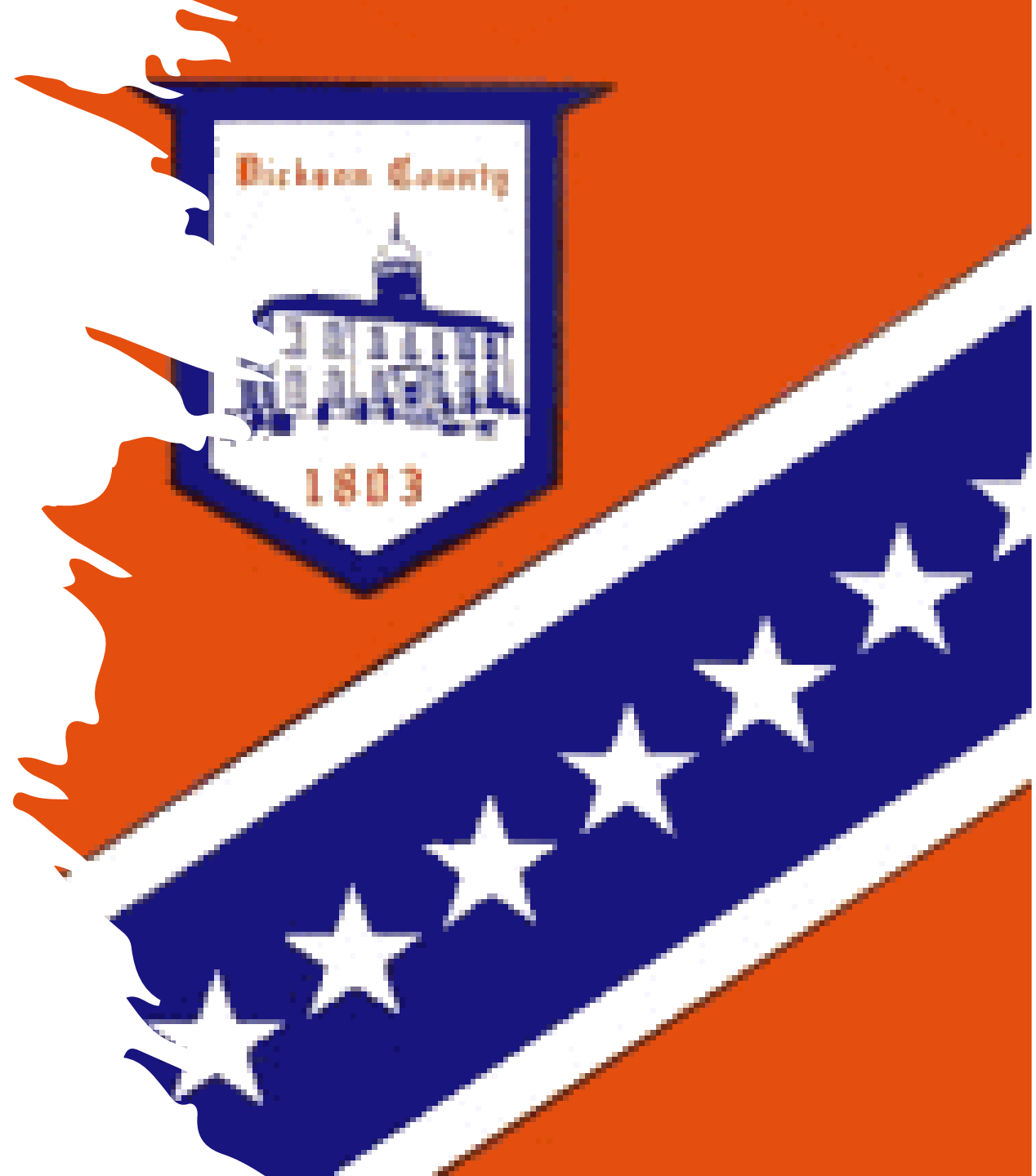


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Dickson County:

White Bluff wwtp

Jones Creek wwtp

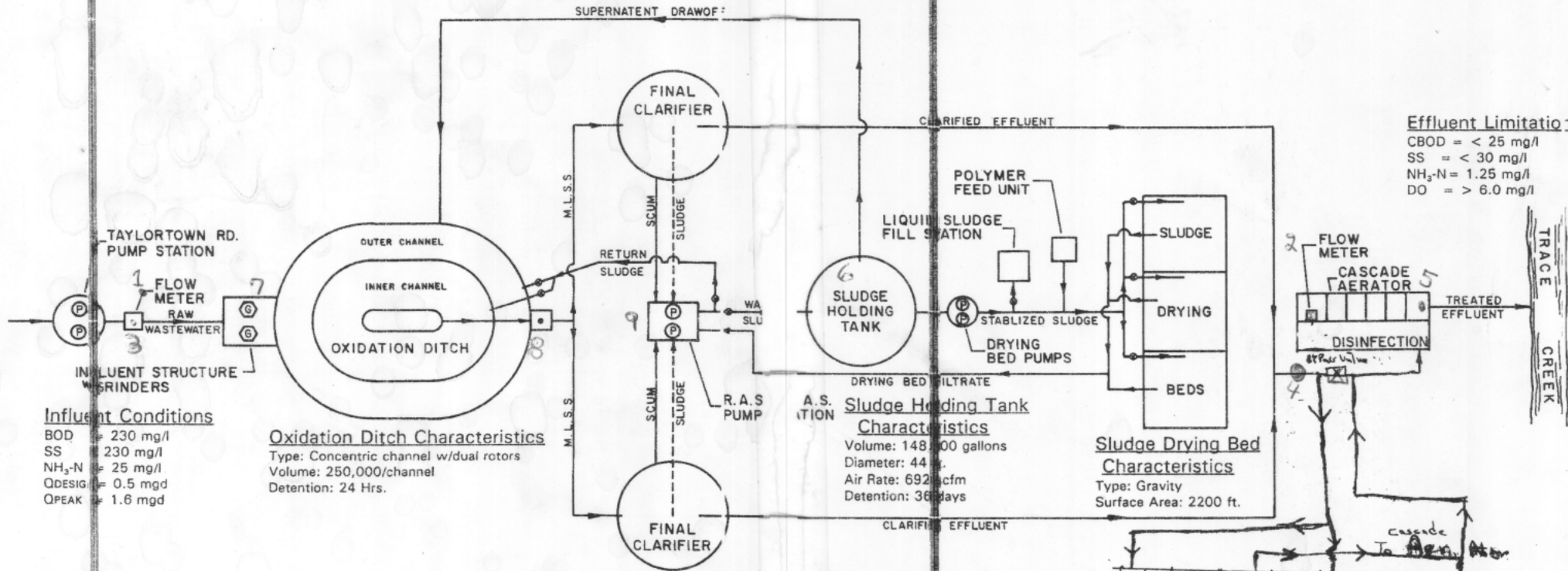






**White Bluff Wastewater Treatment Plant**  
347 Shady Oak Dr.  
White Bluff, Tennessee 37187  
NPDES# TN0020460  
Design Capacity: 0.5 MGD





Effluent Limitations  
 CBOD = < 25 mg/l  
 SS = < 30 mg/l  
 NH<sub>3</sub>-N = 1.25 mg/l  
 DO = > 6.0 mg/l

Influent Conditions  
 BOD = 230 mg/l  
 SS = 230 mg/l  
 NH<sub>3</sub>-N = 25 mg/l  
 QDESIGN = 0.5 mgd  
 QPEAK = 1.6 mgd

Oxidation Ditch Characteristics  
 Type: Concentric channel w/dual rotors  
 Volume: 250,000/channel  
 Detention: 24 Hrs.

Sludge Holding Tank Characteristics  
 Volume: 148,000 gallons  
 Diameter: 44 ft.  
 Air Rate: 692 acfm  
 Detention: 36 days

Sludge Drying Bed Characteristics  
 Type: Gravity  
 Surface Area: 2200 ft.

Clarifier Characteristic  
 Type: Peripheral feed/Central  
 Diameter/Tank: 32 ft.  
 SWD/Tank: 12 ft.  
 Hyd. Loading: 311 gpd/sf

12 Chlorine Contact  
 Tanks 4' x 8' x 8'  
 Baffles In Each Tank  
 6 Tanks each Section

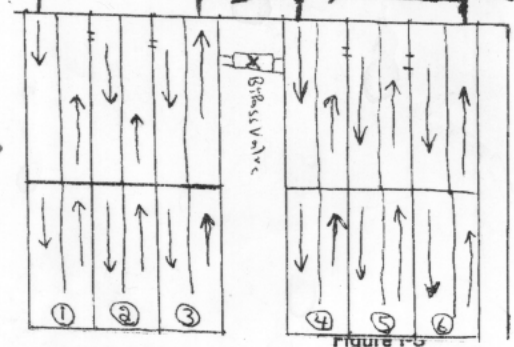
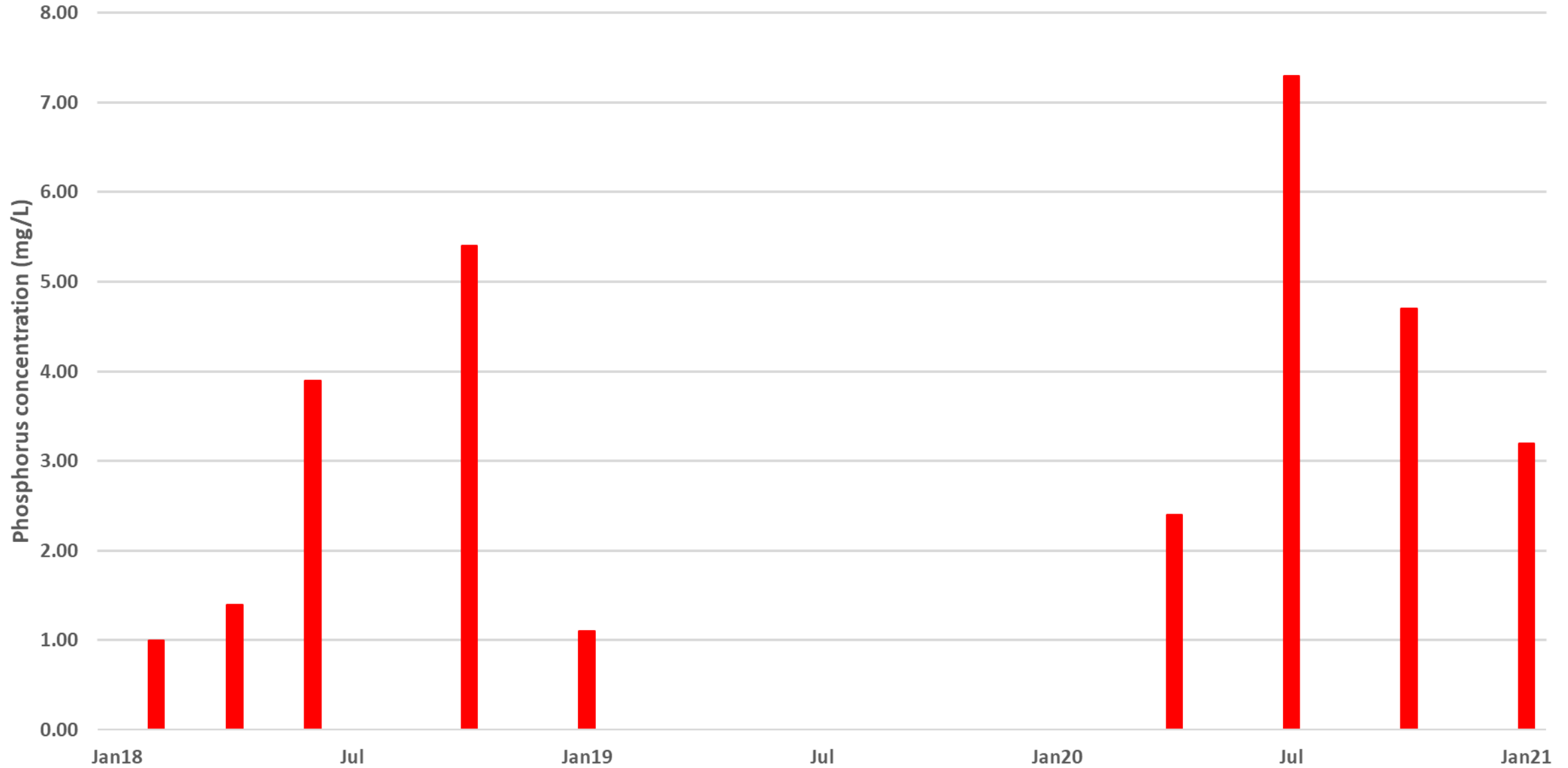


Figure 1-6

**PROCESS FLOW SCHEMATIC**

# Effluent total-Phosphorus White Bluff, Tennessee







Jones Creek wwtp: Dickson, TN

Population: 15,500

4.0 MGD design flow

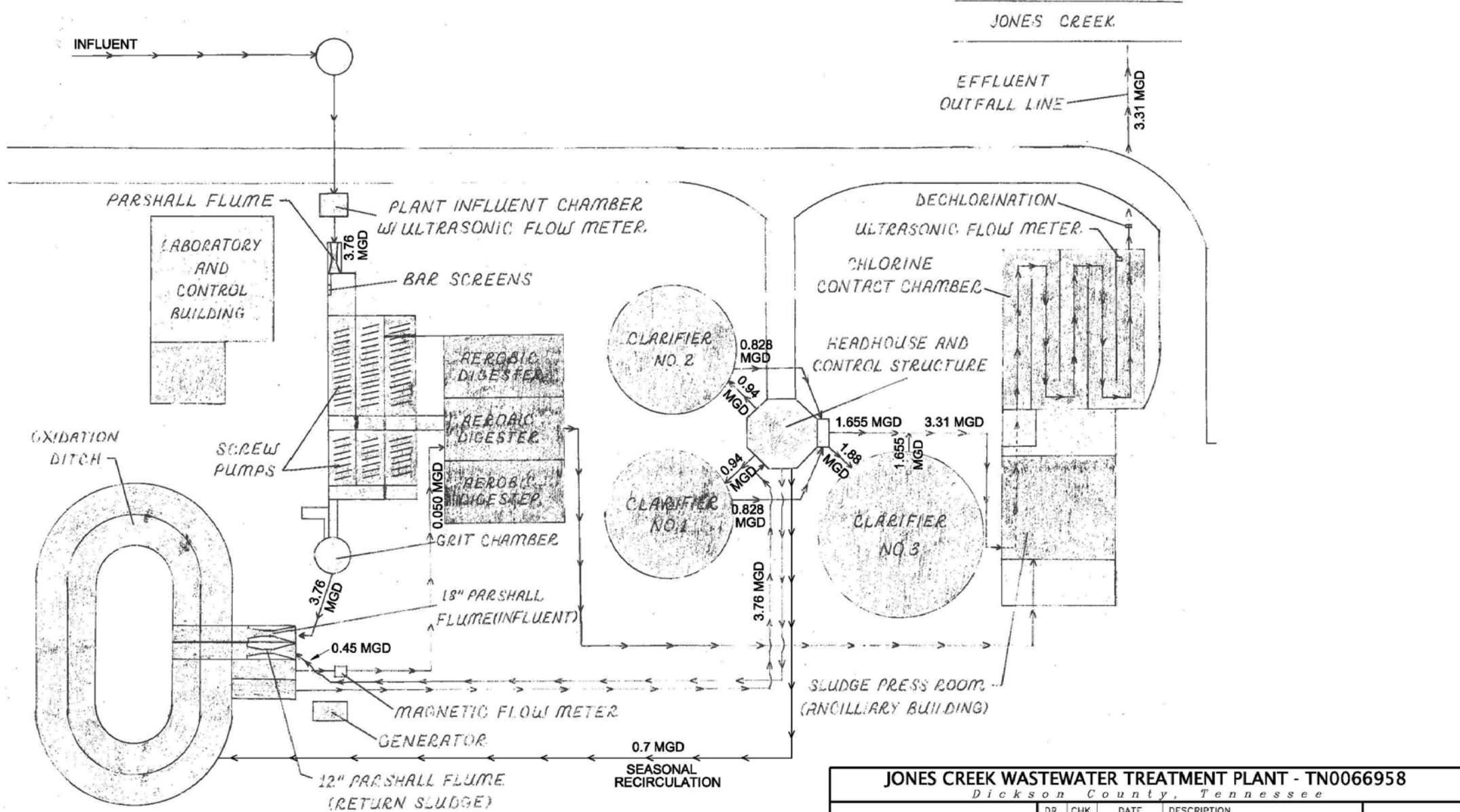












**JCWTP - FLOW SCHEMATIC**  
 Plan Scale: Not To Scale

**JONES CREEK WASTEWATER TREATMENT PLANT - TN0066958**  
*Dickson County, Tennessee*

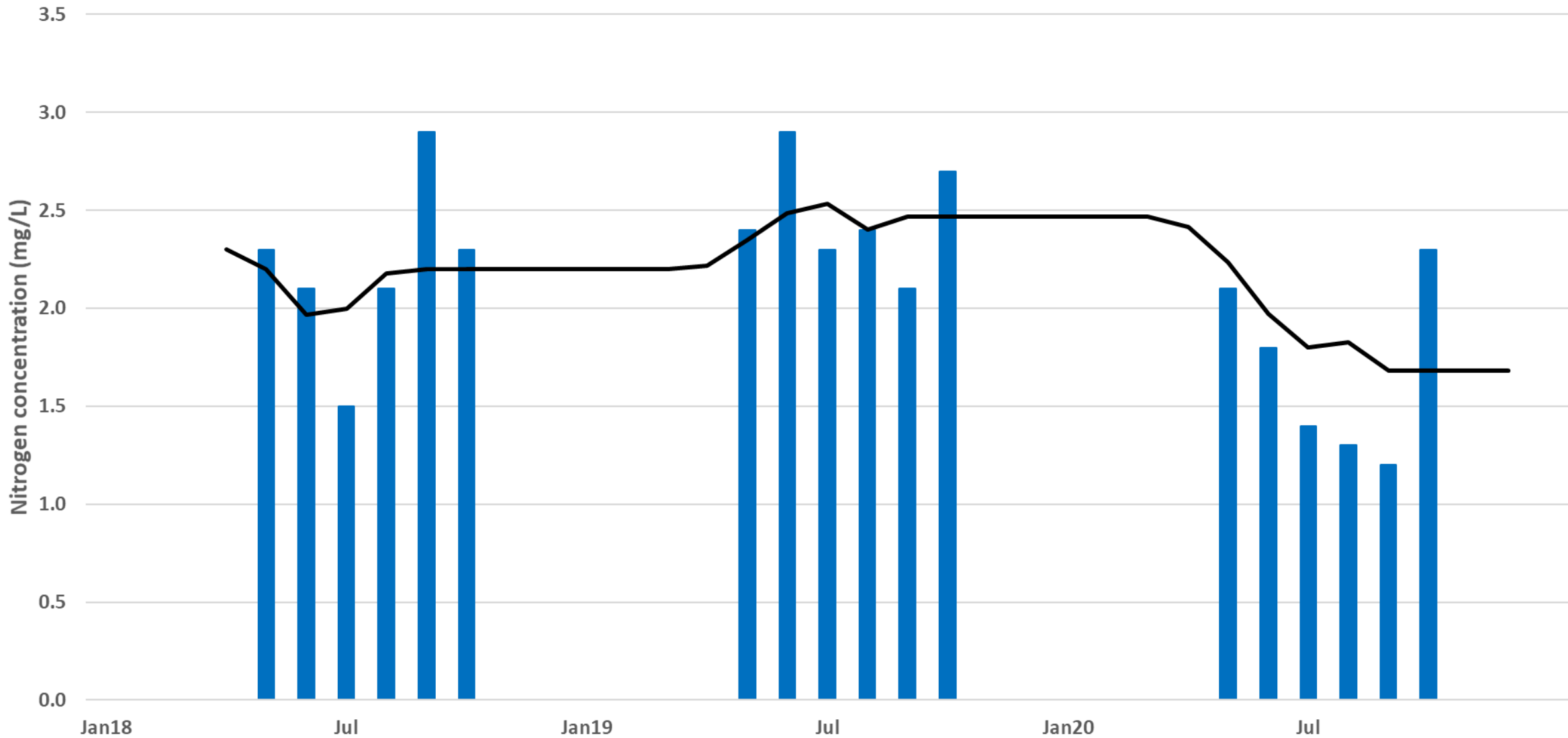
DR.	CHK.	DATE	DESCRIPTION
SBM	SKD	02-22-11	JCWTP SCHEMATIC

**WADC**  
 Water Authority of Dickson County  
 101 Cowan Road • Dickson, Tennessee 37035  
 phone: (615) 441-4188 • www.wadc.us

SCALE: N.T.S.    PROJ. No. S11-002    DWG. No. X-01    **2 of 2**

# Effluent total-Nitrogen Dickson County - Jones Creek

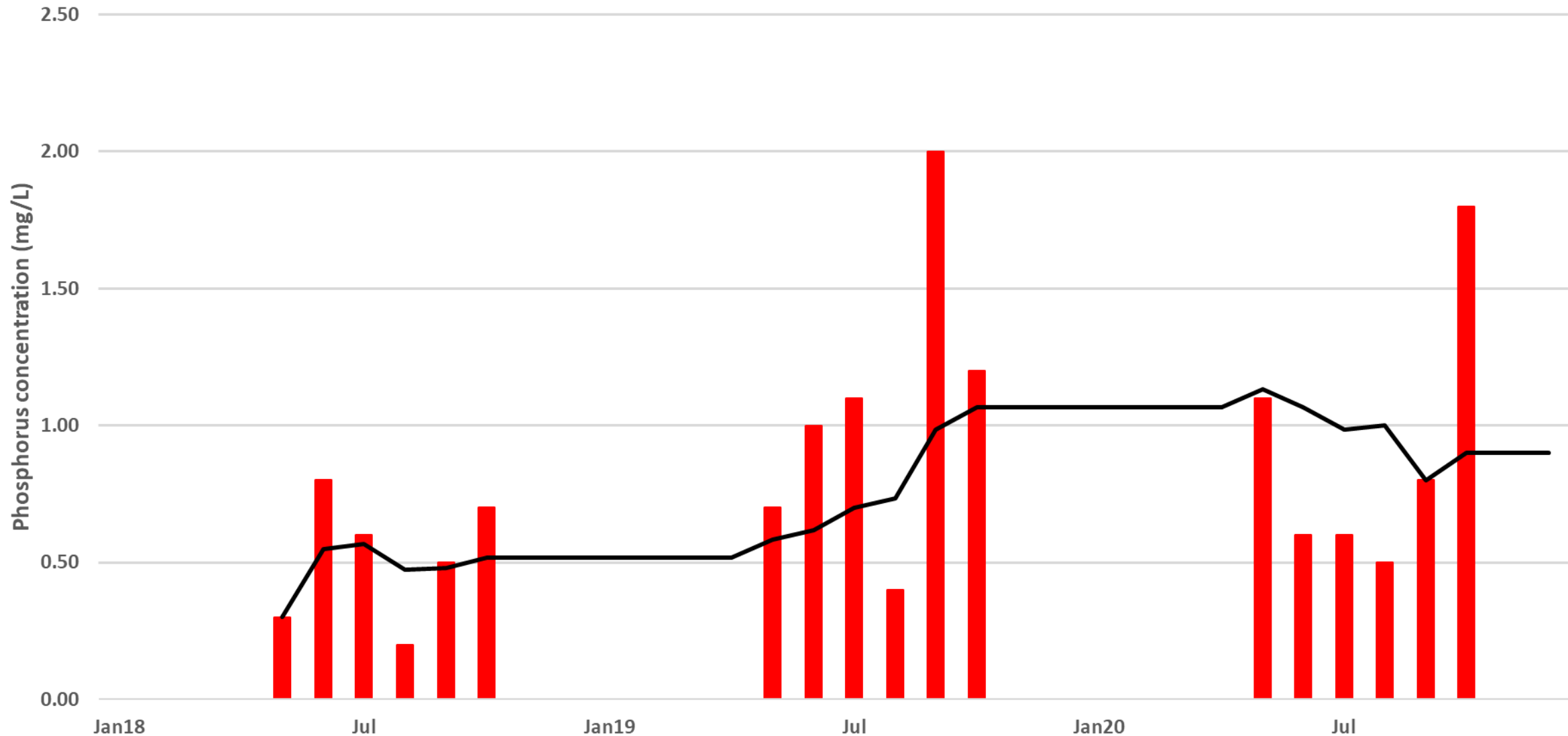
Monthly average tN    Rolling AVG tN





# Effluent total-Phosphorus Dickson County - Jones Creek

total-P Rolling 12-mo AVG



Questions?

Comments?

**Nick Tatum**

ntatum@wadc.us

**Mike Brown**

mbrown@wadc.us

**Kevin Petty**

kpetty@wadc.us





Norris, Tennessee

Population: 1,450

0.2 MGD design flow

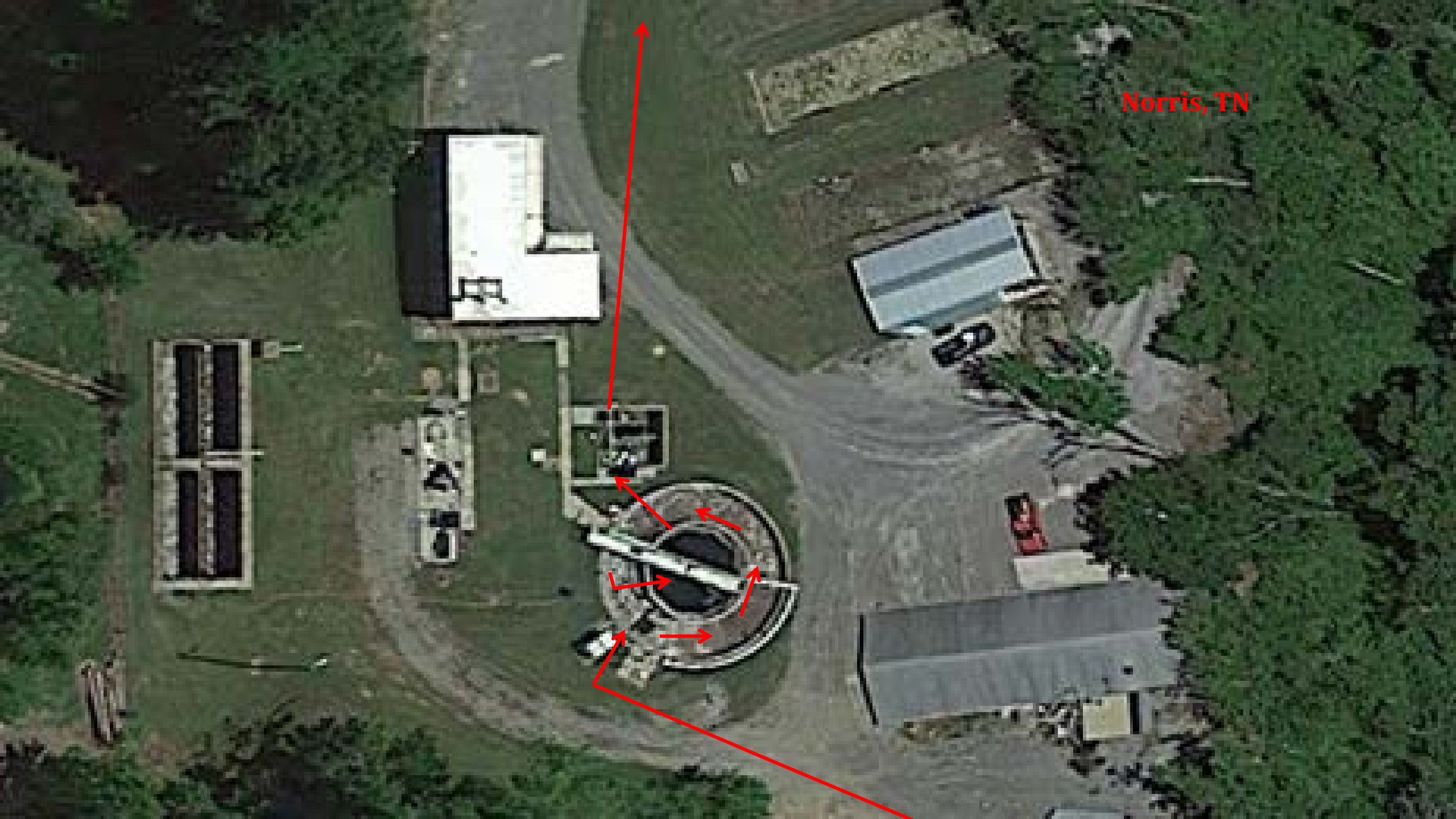


Norris, Tennessee





Norris, TN







**Norris, TN:  
Nitrogen Removal**

**Nitrogen Removal**

Raise MLSS concentration

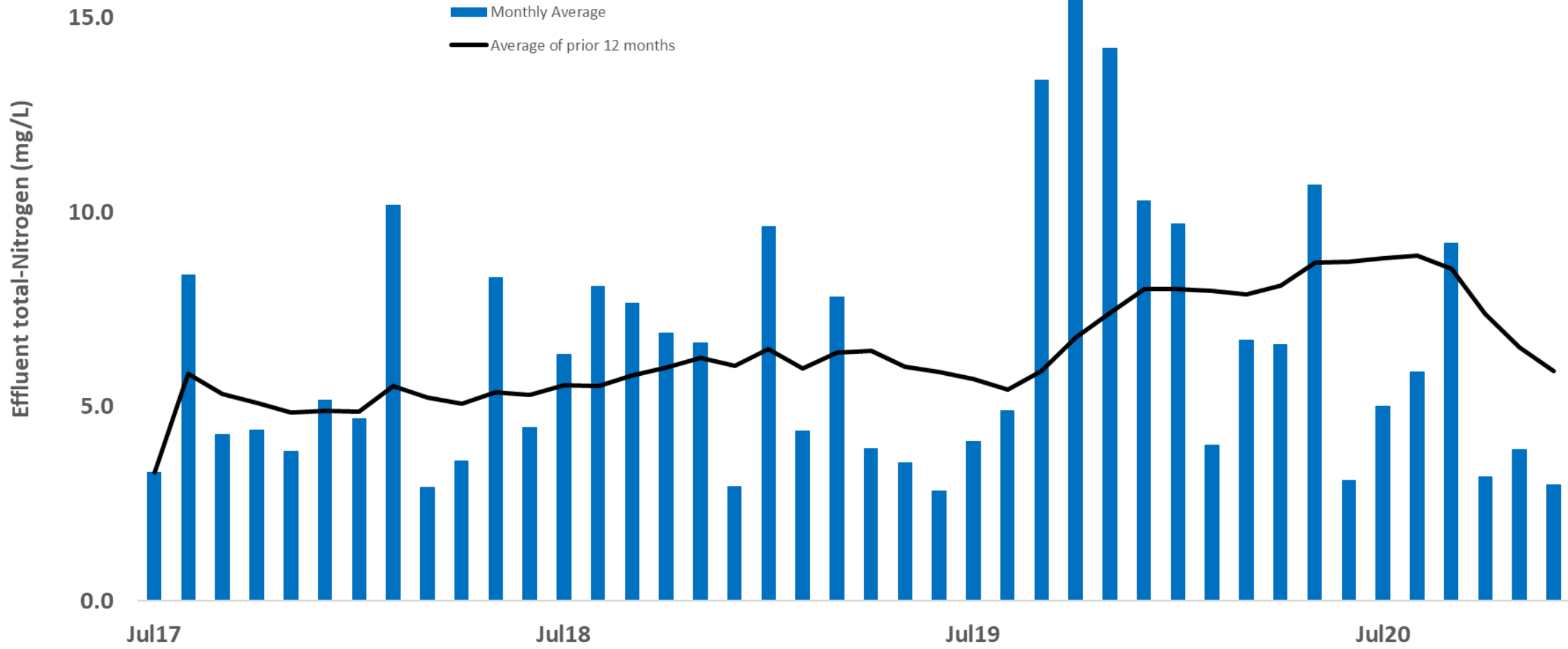
Cycle aeration:

ON 2-3 hours

OFF 1½-2 hours

# Norris, Tennessee

## Effluent Nitrogen: July 2017-2020



**Norris, TN: First try at  
Phosphorus Removal**

**Phosphorus Removal**

Recycle RAS through  
fermenters







**Norris, TN: Second try at Phosphorus Removal**

**Phosphorus Removal**

Create Fermentation Zone in Aeration Tank ...

Air off

70% RAS to aeration



**Norris, TN: Third try at Phosphorus Removal**

**Phosphorus Removal**

Hold influent in tote fermenters

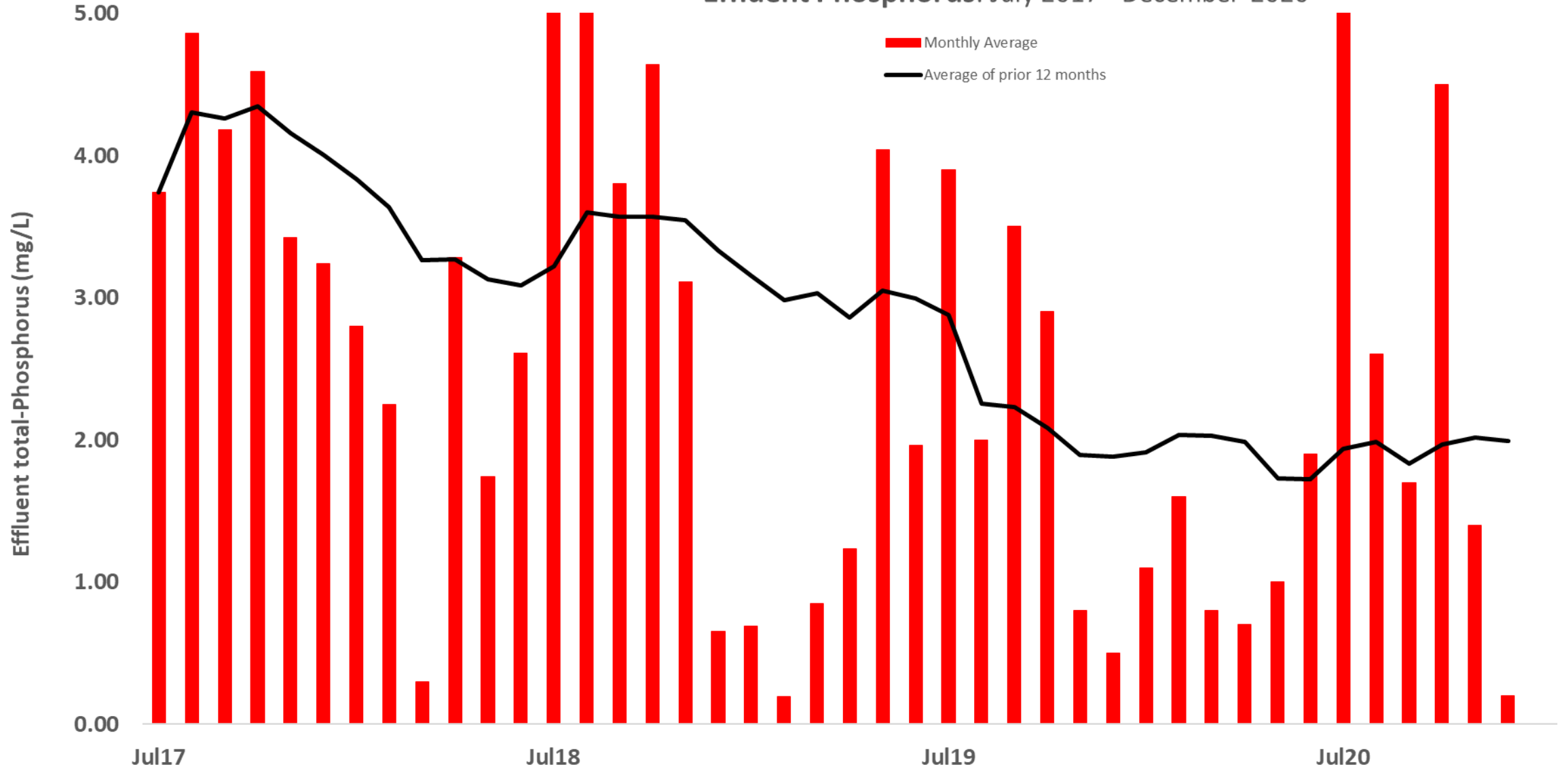
- and -

Create Fermentation Zone in Aeration Tank



# Norris, Tennessee

## Effluent Phosphorus: July 2017 - December 2020



Questions?

Comments?

**Doug Snelson**

Dsnelson.nwc@gmail.com





???



**BREAK TIME**







Harpeth Valley, Tennessee

Population: 25,000

10 MGD design flow

# HVUD WWTP

4063 Old Hickory Blvd

Nashville, TN 37218



# HVUD Plant Design

- Design Flow 10 MGD
- Average Flow ~5 MGD
- Peak Flow 25 MGD
- Hydraulic Retention Time 20 Hours
- Extended Aeration Capacity
  - Anoxic 1.4 MGD
  - Aerobic 6.93 MGD
- Serving over 13,800 Sewer Customer

None

### Gen Power Params

Emerg Generator

Ready

Bkr 52MA  
Closed

Bkr 52G  
Open

Primary  
Electrical Bldg

RAS Flow = 2642 GPM

WW Level = 2.0 Ft

Screw LS

Secondary  
Electrical Bldg

Disinfection Unit

1 Chem Pumps  
2

Plant Flow =  
Plant Press =

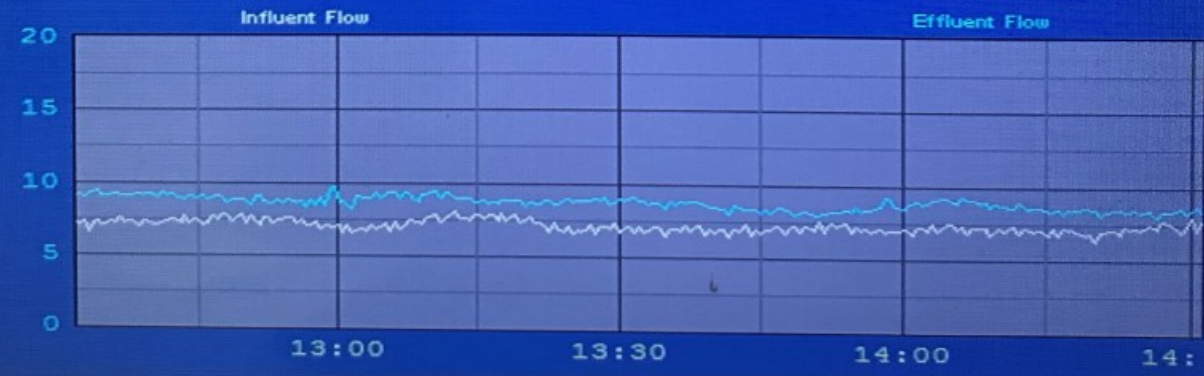
er Params

Power



Influent Flow = 7.015 MGD

ed Overall Creek &  
ump Return  
r Yesterday = 7,140 MG

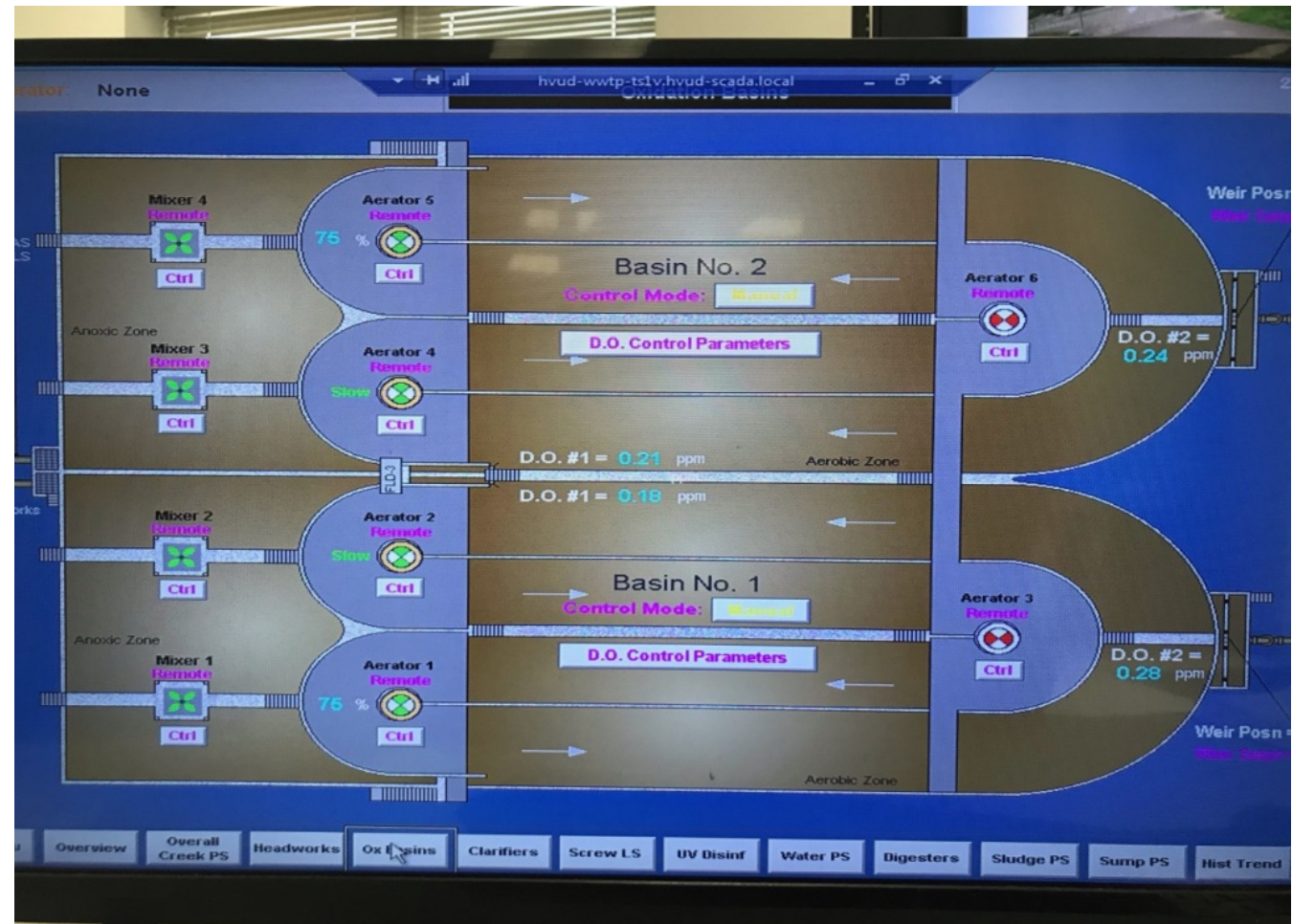


Effluent Flo



# Extended Aeration Operation

- Maintain a D.O. of 0.2-0.9 mg/L
- Limit Aerators in Operation
- On/Off Aeration

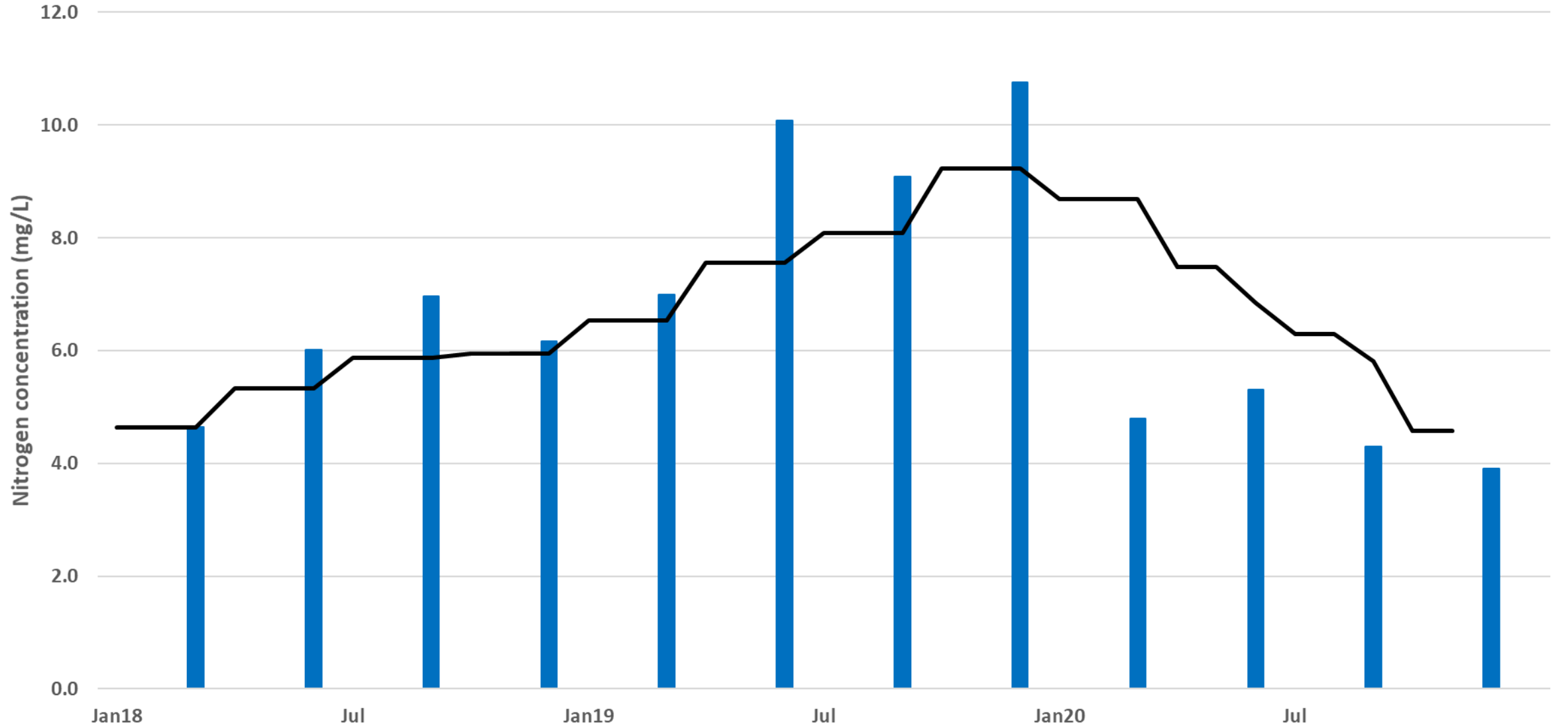


# Nitrogen

- Influent 31.6 mg/L
- Effluent 4.2 mg/L
- Approximately 87% Removal rate

# Effluent total-Nitrogen Harpeth Valley (Nashville), Tennessee

Monthly average tN    Rolling AVG tN



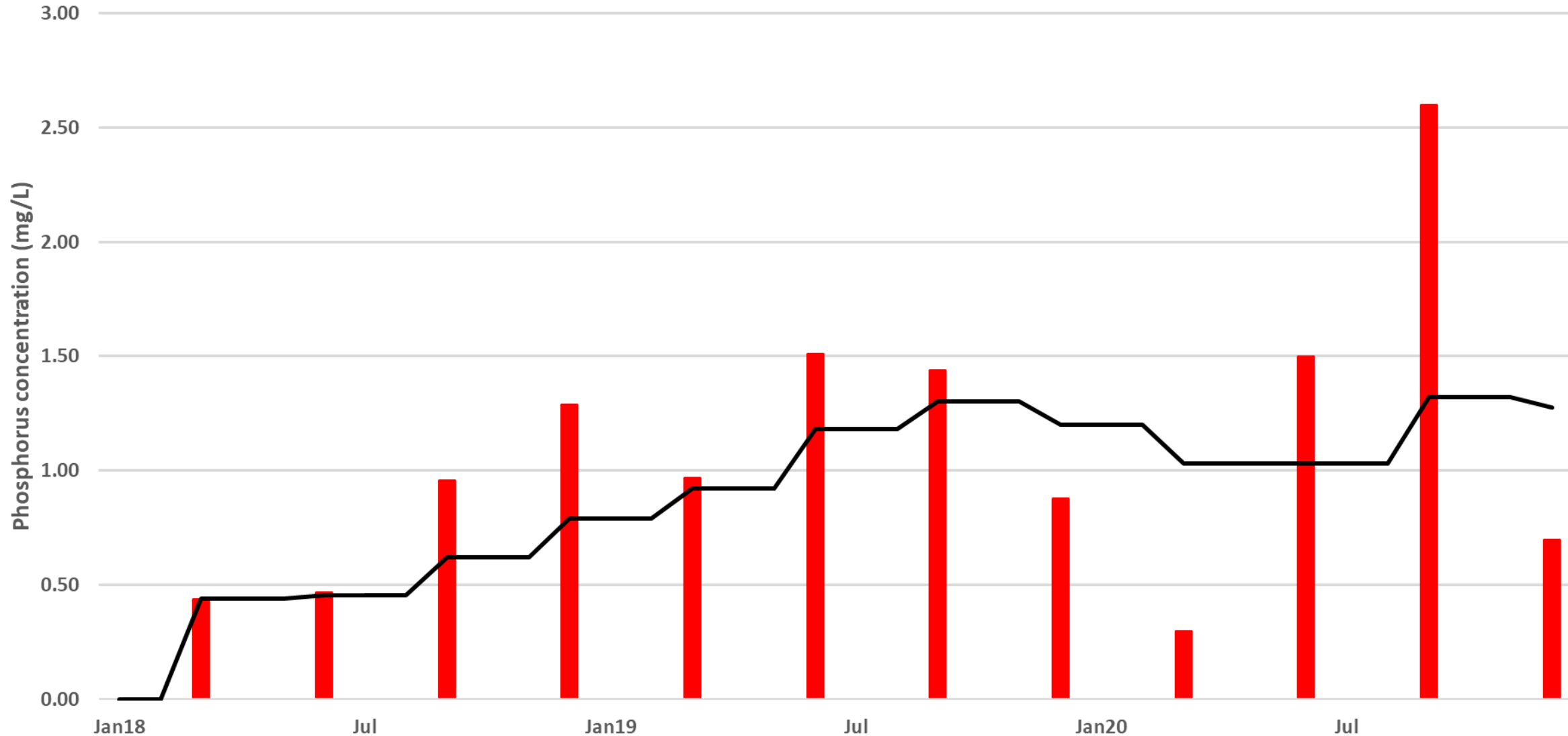


# Phosphorus

- Influent Average 3.4 mg/L
- Effluent Average 1.5 mg/L
- Approximate 56% Removal

# Effluent total-Phosphorus Harpeh Valley (Nashville), Tennessee

total-P Rolling 12-mo AVG



# Objectives

- Find ways to save energy
  - On/Off Air
  - Minimize Aerators in Operation
- Through saving energy, nutrient removal was increased



Questions?

Comments?

**Brad Roberts**

bradroberts@hvud.com

**Albert Solberg**

asolberg@hvud.com



McMinnville, Tennessee

Population: 13,700

4.0 MGD design flow



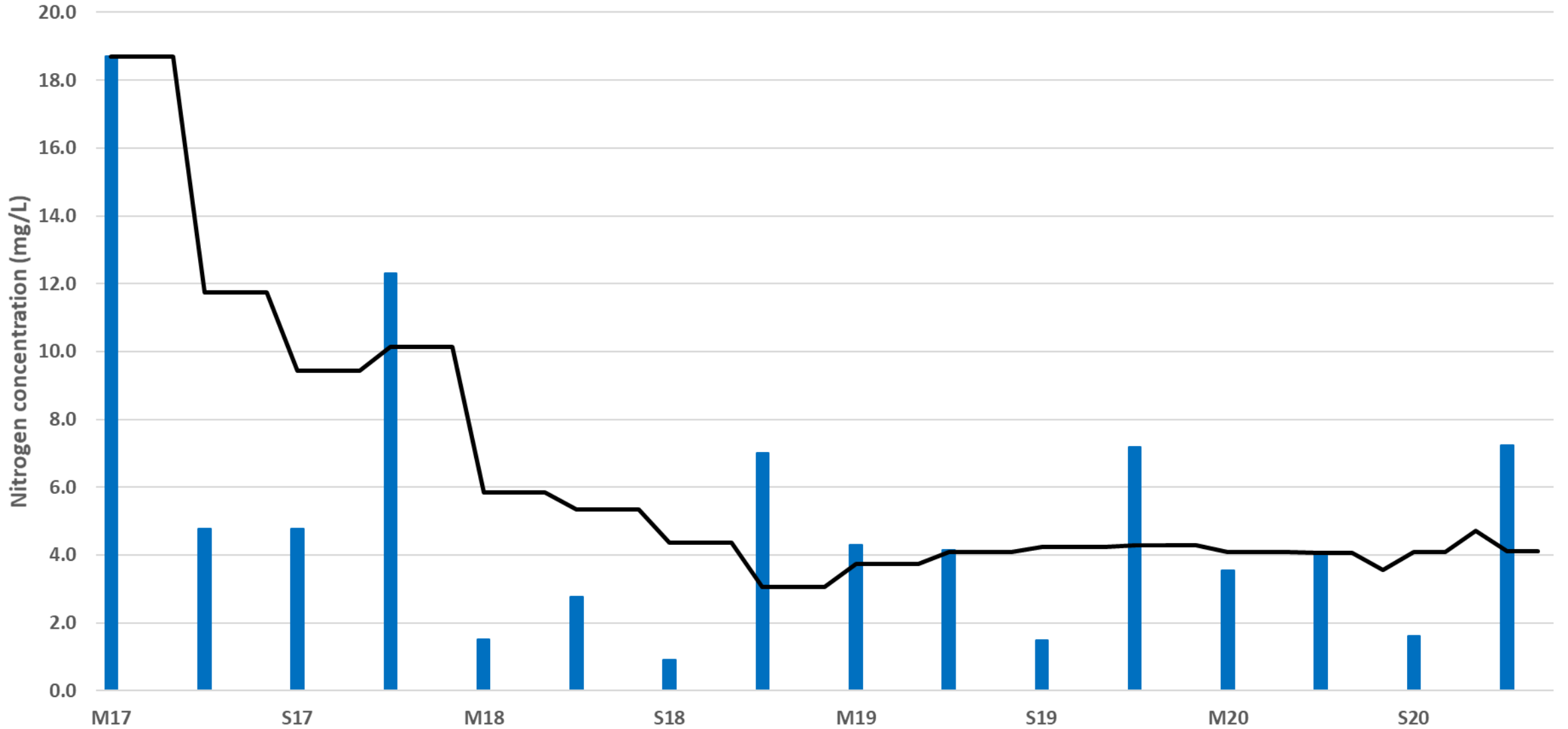


Clark Creek



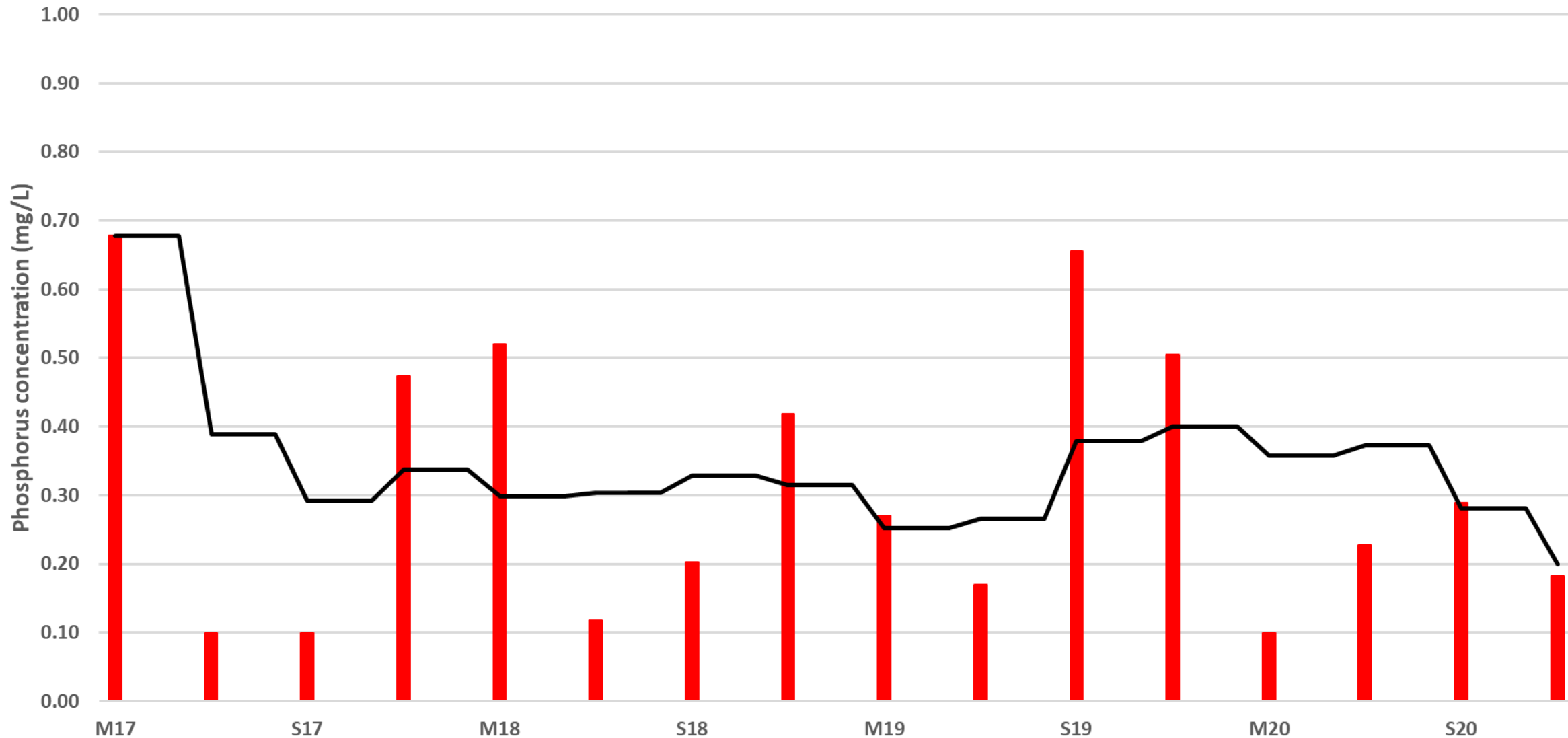
# Effluent total-Nitrogen McMinnville, Tennessee

Monthly average tN    Rolling AVG tN



# Effluent total-Phosphorus McMinnville, Tennessee

total-P Rolling 12-mo AVG



Questions?

Comments?

**Phil Miller**

[pmiller@mcminnvilletn.gov](mailto:pmiller@mcminnvilletn.gov)



## Acknowledgements

### **TENNESSEE DEPARTMENT OF ENVIRONMENT & CONSERVATION (TDEC)**

Karina Bynum, Sherry Wang, George Garden, Jenny Dodd, Jason Benton, Eddie Bouzied, Bryan Carter, David Duhl, Jordan Fey, Oakley Hall, Michael Murphy, Steve Owens, Rob Ramsey, Sherwin Smith, Robert Tipton, Sandra Vance, John West, Ariel Wessel-Fuss ...

### **HARRIMAN**

Ray Freeman

### **NASHVILLE**

Johnnie MacDonald & David Tucker

### **NORRIS**

Tony Wilkerson & Doug Snelson

Brett Ward (UT-MTAS), Dewayne Culpepper (TAUD), Greg Hayes (Athens), Larry Gamblin (Bartlett), Danny Neely (Baileyton), David Harrison (Collierville), Nic Willis (Cowan), Ray Freeman (Harriman), Darryl Green (Henderson), Jack Hauskins & Rocky Hudson (Lafayette), Johnnie MacDonald (Nashville) ...

... and, many more!



## Acknowledgements, continued

**KANSAS** Tom Stiles, Rod Geisler (retired), Shelly Shores-Miller, Nick Reams & Ryan Eldredge (**KDHE**), Jamie Belden & Becky Lewis (**Wichita**)

**MONTANA** Paul LaVigne (retired), Pete Boettcher, Josh Viall, Ryan Weiss, Bill Bahr (retired), Dave Frickey (retired) & Mike Abrahamson (**DEQ**), Keith Thaut (**Conrad**), Mark Fitzwater & entire staff (**Helena**)

**EPA** Paul Shriner & Tony Tripp (**HQ**), Tina Laidlaw (**R8**), Brendon Held & Craig Hesterlee (**R4**), Sydney Weiss (**R5**)

... and, many more!





???



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Comments &  
Questions





Questions?

Comments?

Grant Weaver  
g.weaver@cleanwaterops.com



**REVENUE**

Change day-to-day operations to create ideal habitats for bacteria to remove phosphorus



7

**N**

**Nitrogen**



## ***Step 1: Convert Ammonia ( $NH_4$ ) to Nitrate ( $NO_3$ )***

Oxygen-rich Aerobic Process

Don't need BOD for bacteria to grow

Bacteria are sensitive to pH and temperature

## ***Step 2: Convert Nitrate ( $NO_3$ ) to Nitrogen Gas ( $N_2$ )***

Oxygen-poor Anoxic Process

Do need BOD for bacteria to grow

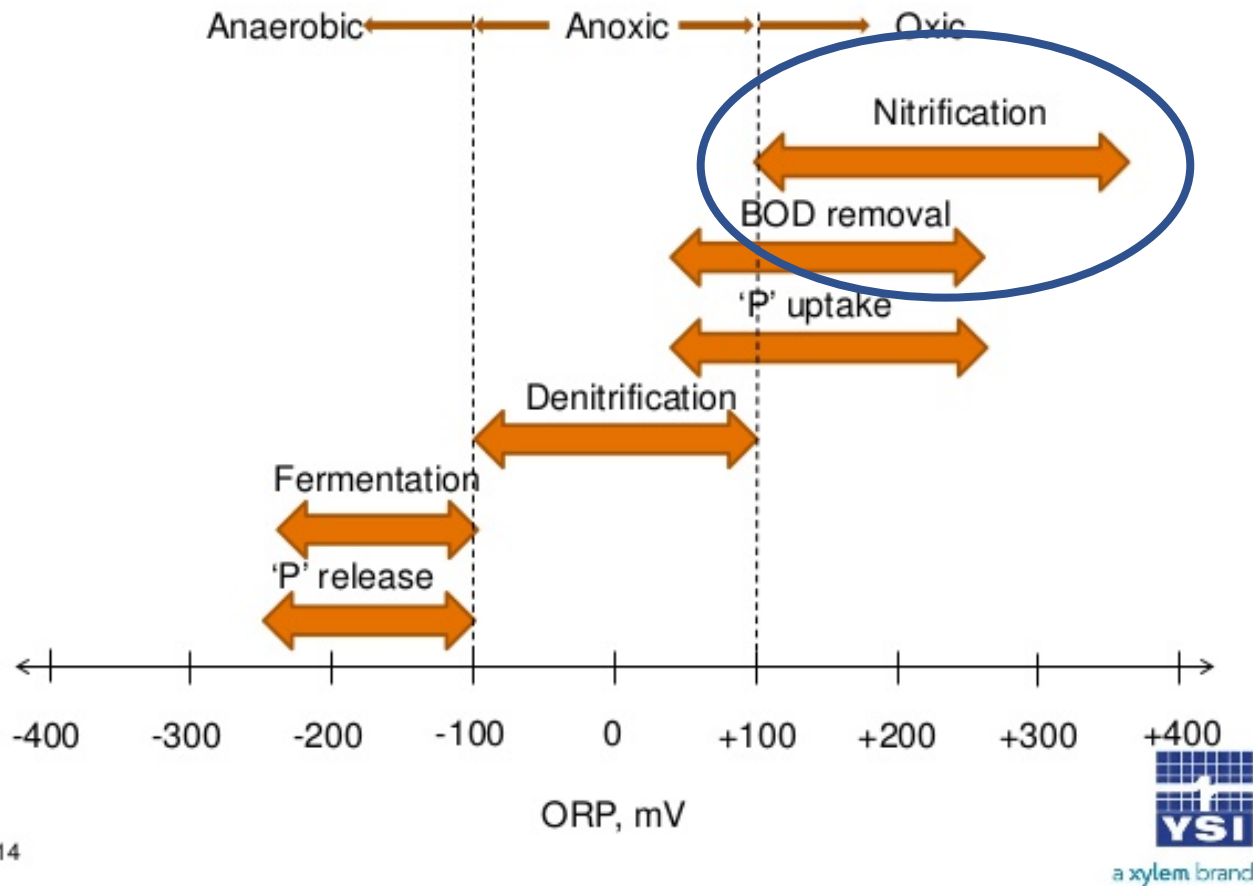
Bacteria are hardy



# Ammonia Removal - 1<sup>st</sup> Step of N Removal

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## What Does ORP Tell Us About Our Process?



### Step 1: Ammonia Removal

7

pH of 6.5+

Plenty of Dissolved Oxygen (DO) /L

ORP of +150 mV

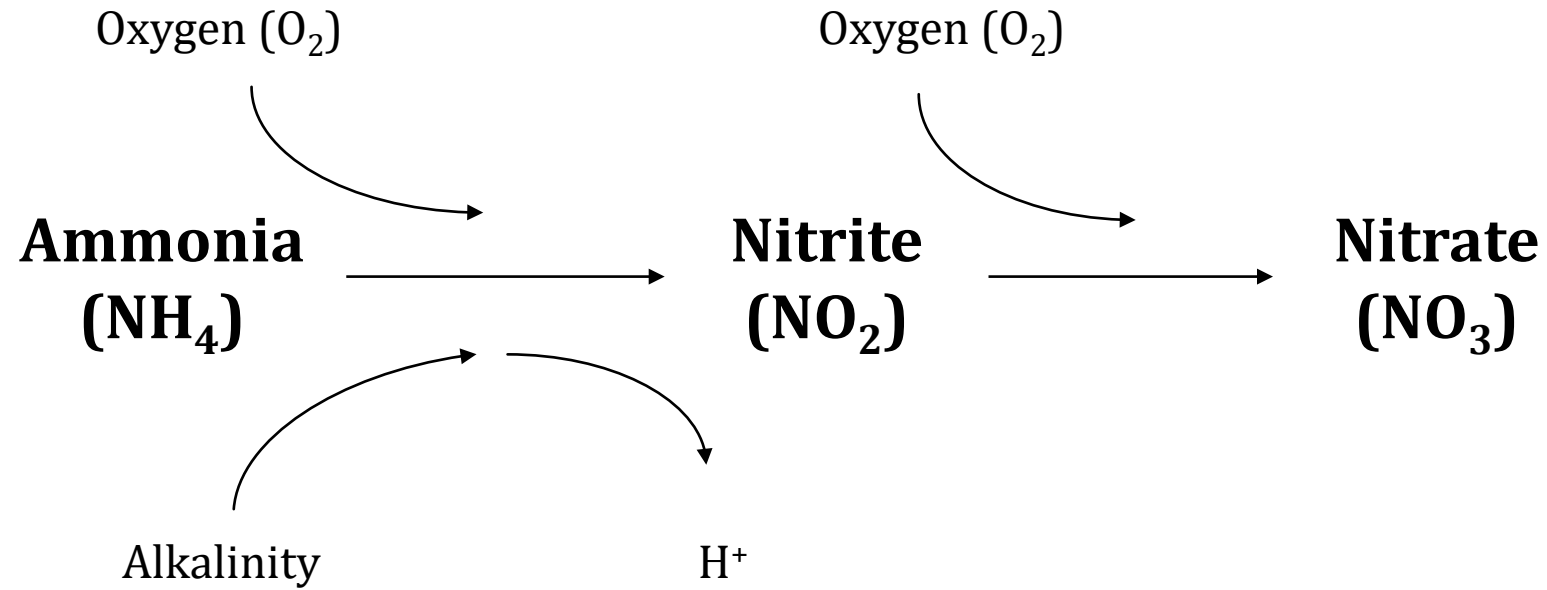
Little to no BOD

4+ hours retention time

**Nitrogen**



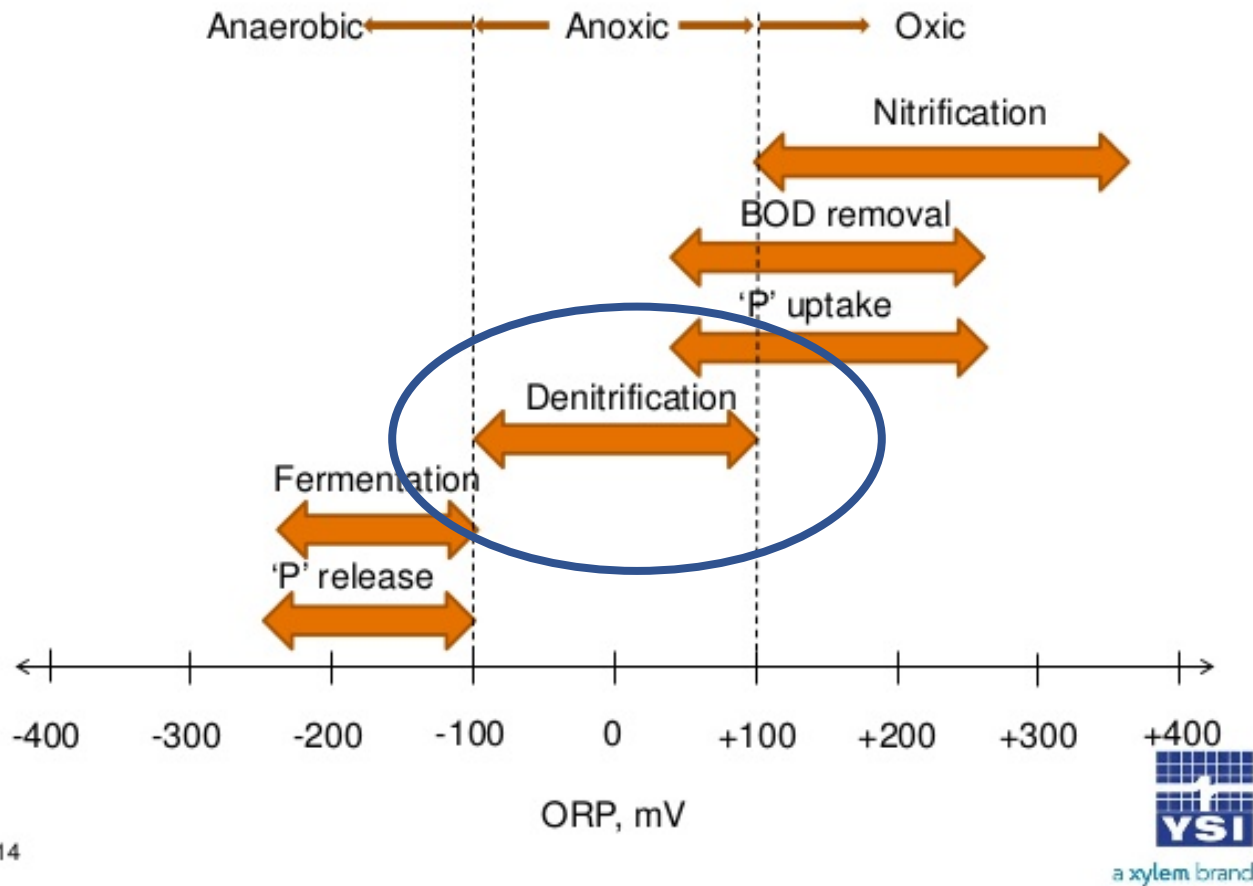
# Ammonia Removal



Nitrate  
Removal - 2<sup>nd</sup>  
Step of N  
removal



## What Does ORP Tell Us About Our Process?



14

7

Step 2: Nitrate Removal

Little to no nitrification

ORP of -100 mV

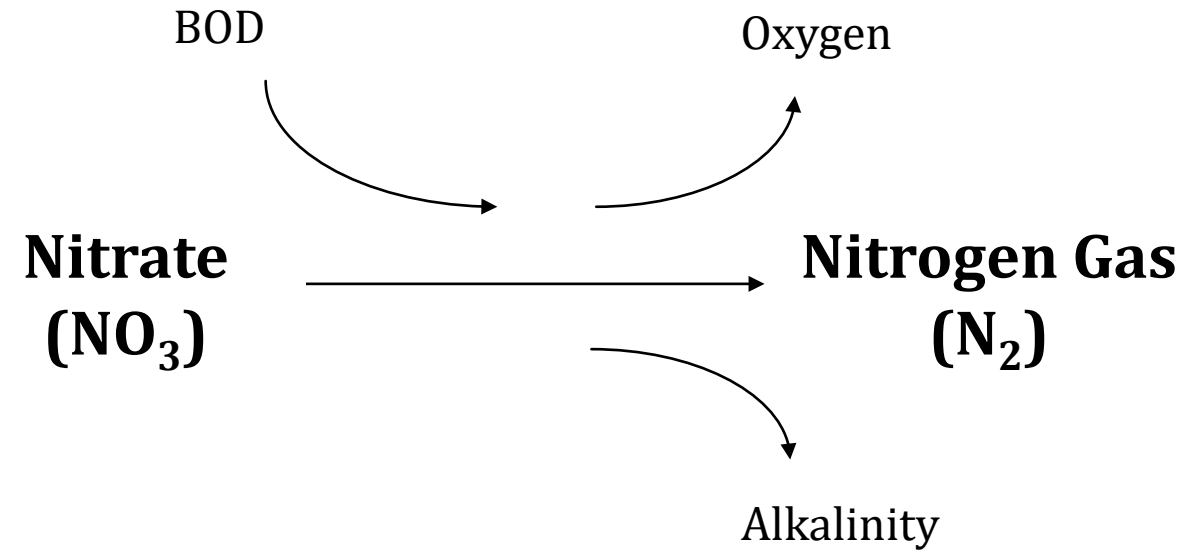
5-10 times as much as Nitrate

2+ hours retention time

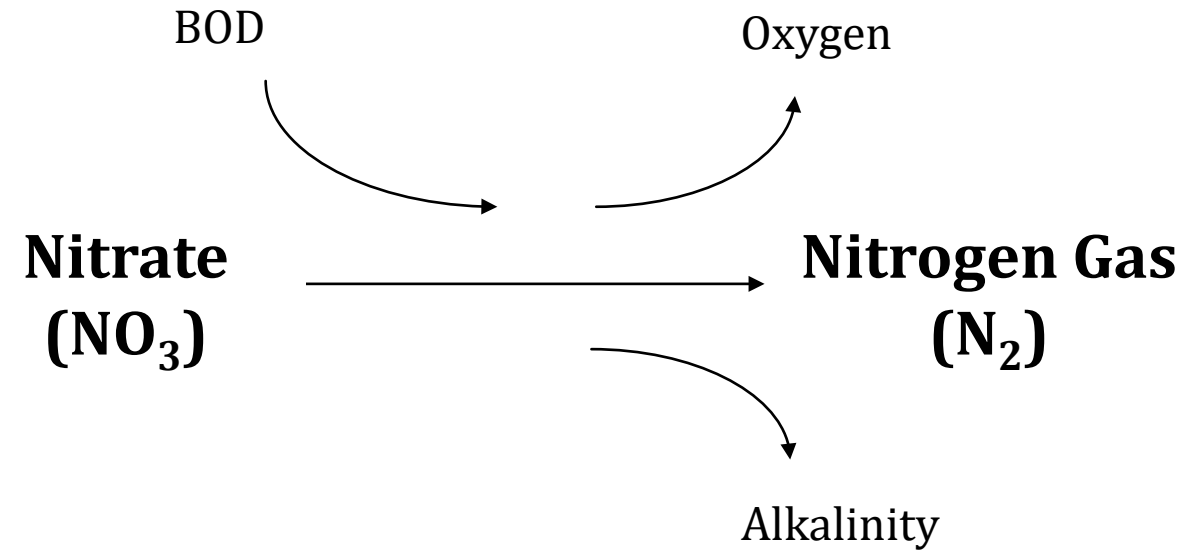
# Nitrogen



# Nitrate Removal



# Nitrate Removal



Adds DO (dissolved oxygen)

Consumes BOD ... **Denitrifiers out compete bio-P bugs for VFAs!**

Gives back alkalinity ... **beneficially raises pH**

# *Nitrogen Removal*

	<b>Step 1: Nitrification</b> (Ammonia Removal)	<b>Step 1: Denitrification</b> (Nitrate Removal)
DO: Dissolved Oxygen	1 mg/L or more	Less than 0.2 mg/L
ORP: Oxygen Reduction Potential	+150 mV	-100 mV
MLSS: Mixed Liquor Suspended Solids	2500 mg/L or more	Same
HRT: Hydraulic Retention Time	6 or more hours	1 or more hours
<b>BOD: Biochemical Oxygen Demand</b>	less than 20 mg/L	<b>100 mg/L or more ... VFAs preferred!</b>
Alkalinity	60 mg/L or more <i>Alkalinity is lost</i>	<i>Alkalinity is gained</i>

Note: All numbers are approximations, “rules of thumb”

Questions?

Comments?

Grant Weaver  
g.weaver@cleanwaterops.com



Phosphorus

15

P

30.974

# THREE steps



# ***Biological Phosphorus Removal***

Step 1: prepare “dinner”

VFA (volatile fatty acids) production in anaerobic/fermentive conditions

# Phosphorus

15

Step 1: VFA Production

ORP of -200 mV or more negative

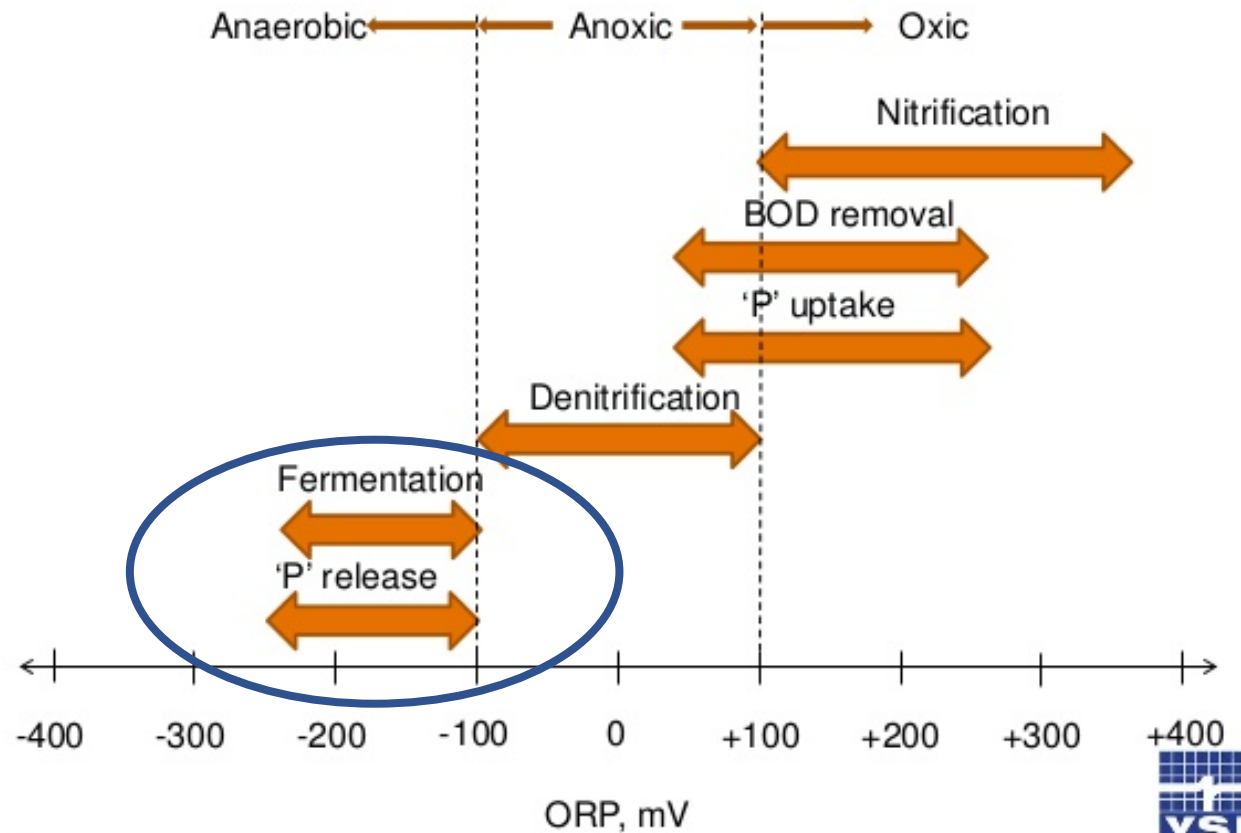
25 times as much BOD as orthophosphate

Retention time ... long enough to go septic

P

30.974

## What Does ORP Tell Us About Our Process?





# ***Biological Phosphorus Removal***

## Step 1: prepare “dinner”

VFA (volatile fatty acids) production in anaerobic/fermentive conditions

## Step 2: “eat”

Bio-P bugs (PAOs, “phosphate accumulating organisms”) eat VFAs in anaerobic/fermentive conditions ... temporarily releasing more P into the water

# Phosphorus

15

Step 2: VFA uptake / P-release

MLSS and VFAs in same tank

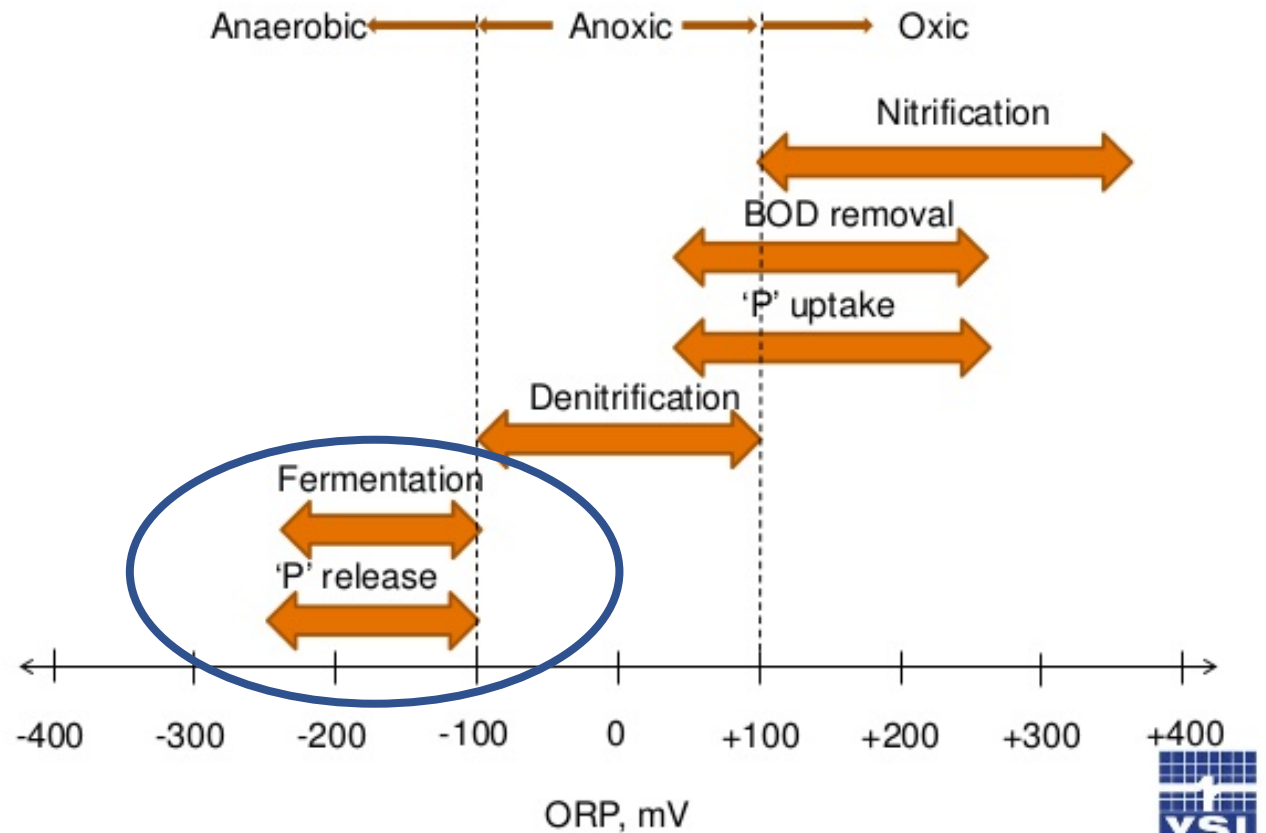
ORP of -200 mV or more negative

Nitrate control

Process control tool: 3 times as much ortho-P leaving tank as coming in

30.974

## What Does ORP Tell Us About Our Process?



# ***Biological Phosphorus Removal***

## Step 1: prepare “dinner”

VFA (volatile fatty acids) production in anaerobic/fermentive conditions

## Step 2: “eat”

Bio-P bugs (PAOs, “phosphate accumulating organisms”) eat VFAs in anaerobic/fermentive conditions ... temporarily releasing more P into the water

## Step 3: “breathe” and grow

Bio-P bugs (PAOs) take in almost all of the soluble P in aerobic conditions as they grow and reproduce

# Phosphorus

15

Step 3: P-uptake

ORP of +150 mV — no more DO than for ammonia removal

pH of 7.0+

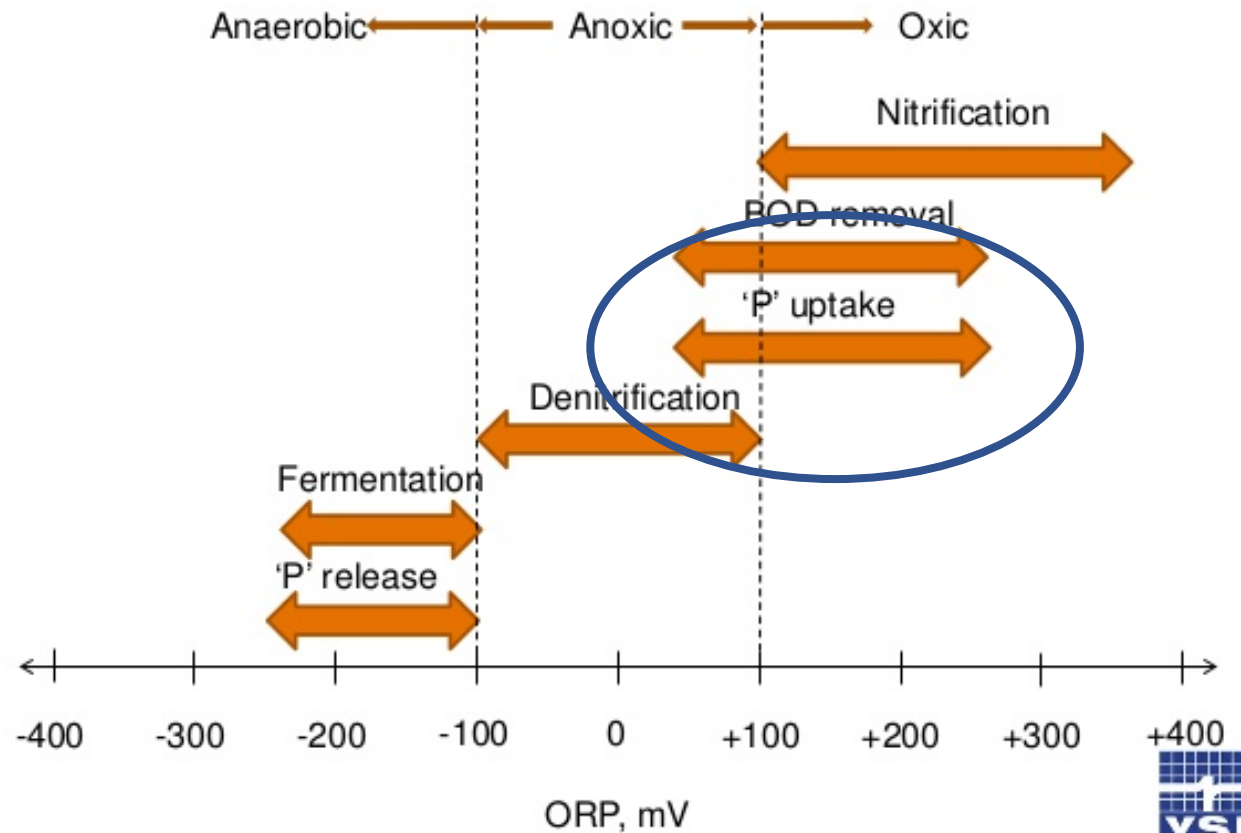
Retention time ... enough to remove ammonia

Enough BOD to support bacteria growth

P

30.974

## What Does ORP Tell Us About Our Process?





# ***Optimizing Bio-P Removal: Mainstream or Sidestream Fermentation***

## **Anaerobic Tank**

2 hour HRT (hydraulic retention time)\*

ORP of -200 mV\*

25 times as much BOD as influent ortho-P\*

Ortho-P release (3 times influent ortho-P)\*

## **Aeration Tank**

DO of 2.0 mg/L

ORP of +150 mV

pH of 7.0+\*

Ortho-P concentration of 0.05 mg/L\*

\*Approximate: Every Plant is Different

Questions?

Comments?

Grant Weaver  
g.weaver@cleanwaterops.com





Murfreesboro, Tennessee

Population: 136,000

20 MGD design flow







Fleming Training Center

Murfreesboro Waste Water Plant

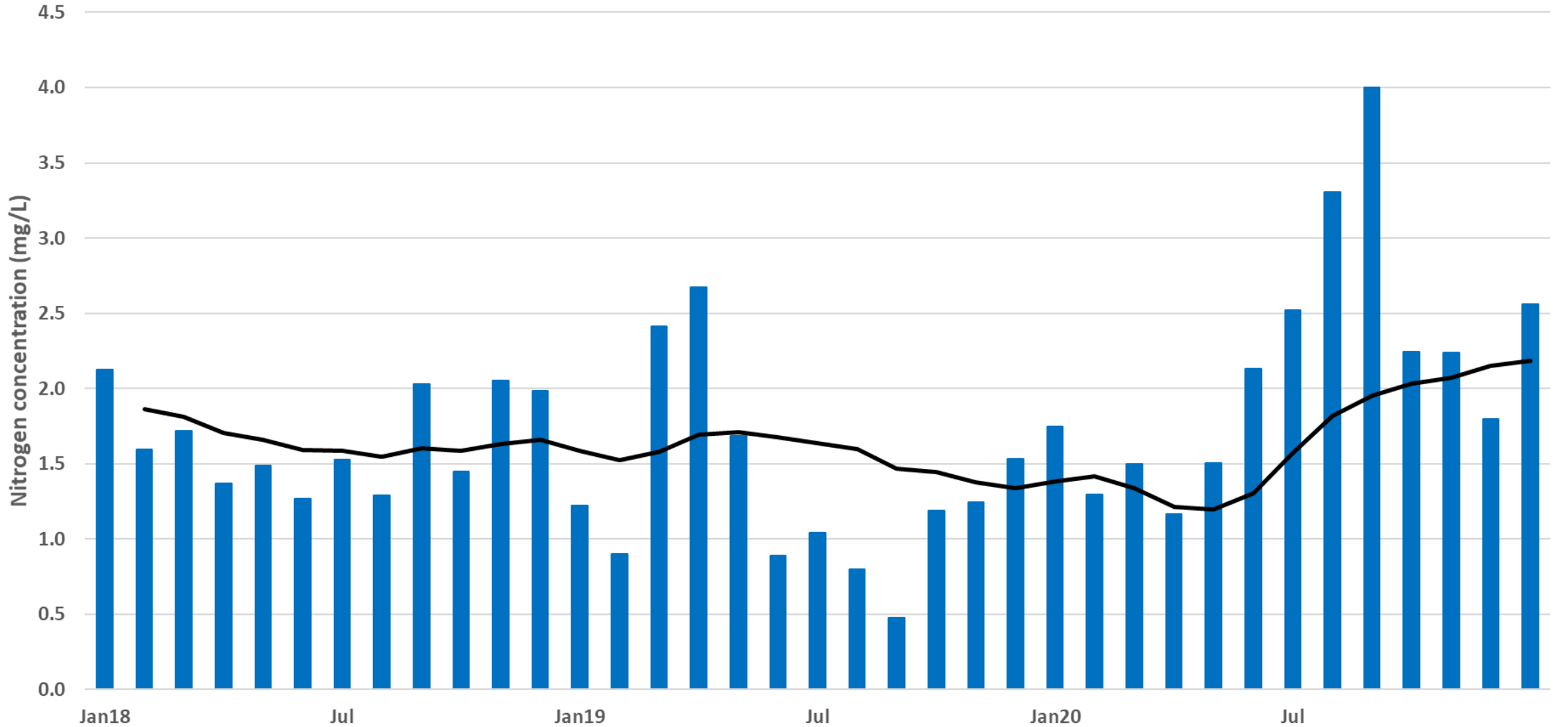
Blanton Dr

Blanton Dr



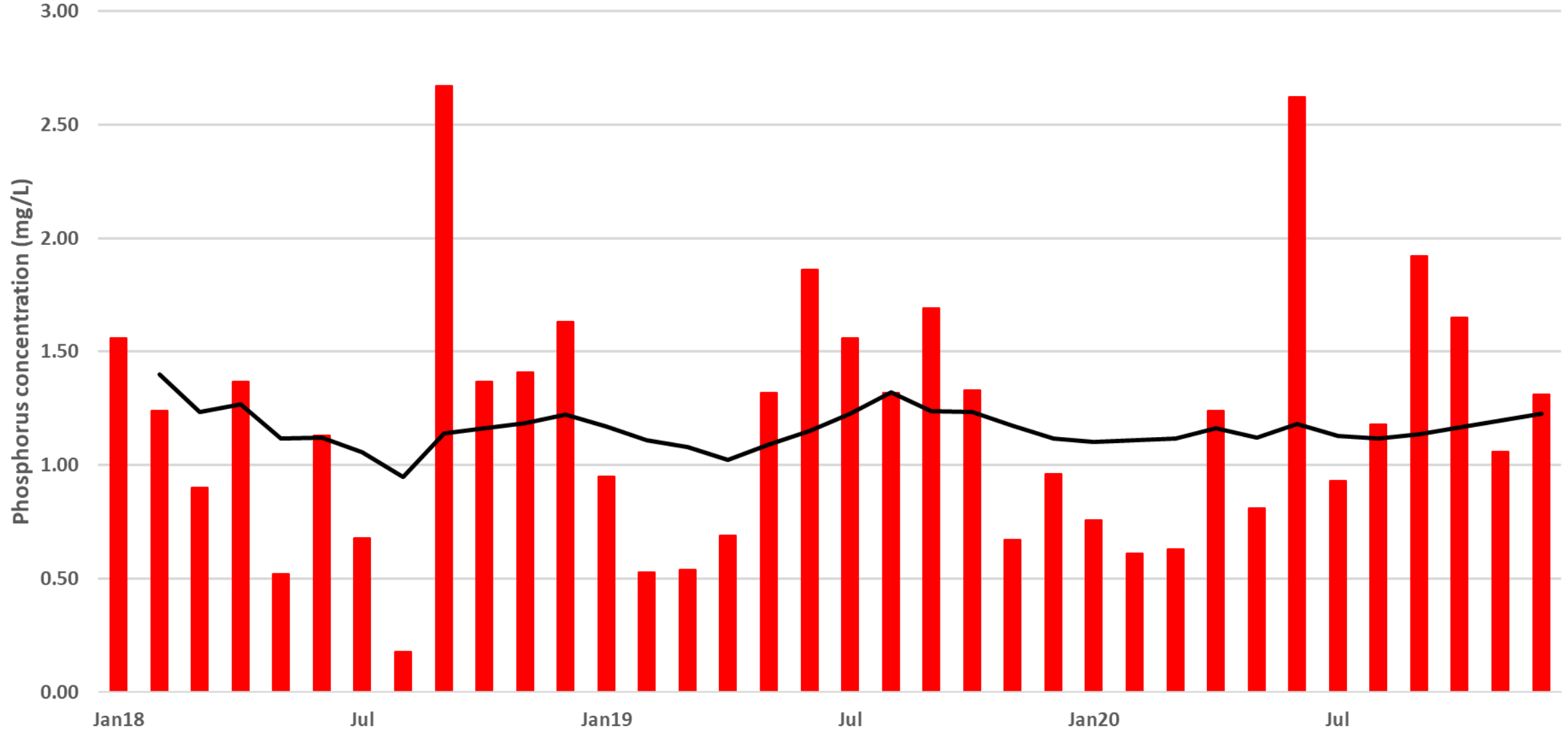
# Effluent total-Nitrogen Murfreesboro, Tennessee

Monthly average tN    Rolling AVG tN



# Effluent total-Phosphorus Murfreesboro, Tennessee

total-P Rolling 12-mo AVG



Questions?

Comments?

Grant Weaver  
g.weaver@cleanwaterops.com